IN THE CLAIMS

Please amend the claims as follows:

Claims 1-17 (Canceled)

18. (Previously Presented) A process for the production of an alkyl-substituted butenol having the formula (I):

$$R^1$$
-CH₂-CH=CR²-CH₂OH (I)

wherein R¹ is a saturated or olefinically unsaturated alkyl or cycloalkyl group having from 4 to 16 carbon atoms and wherein R¹ is optionally substituted by an alkyl, cycloalkyl, aryl or alkaryl having up to 12 carbon atoms; and R² is hydrogen or an alkyl group having from 1 to about 6 carbon atoms the process comprising:

by reacting at least one aldehyde of the formula (II) with at least one corresponding lower aldehyde:

and R¹ has the same meaning as in formula (I); wherein:

- (i) aldol condensation is carried out in an inert organic solvent, and
- (ii) reduction of the unsaturated aldehydes is carried out in the presence of an optionally calcined copper/zinc catalyst, and is carried out continuously under isothermal conditions at a temperature ranging from 45 to 60°C and under a hydrogen pressure of 1 to 300 bar at an LHSV (liquid hourly space velocity) of 0.3 to 3.0 hr⁻¹.
- 2 19. (Previously Presented) The process of claim 18, wherein the aldol condensation is carried out in a nonpolar organic solvent which can form an azeotrope with water.

- 3 20. (Previously Presented) The process of claim 18, wherein the aldol condensation is carried out in the presence of a catalyst which is an ammonium salt of an organic acid.
- 4 21. (Previously Presented) The process of claim 18, wherein R² in formula (I) is a methyl group.
- 5 22. (Previously Presented) The process of claim 18, wherein R² in formula (I) is a methyl group and wherein propional dehyde is used in a 2.5 to 10-fold molar excess based on the aldehyde of formula (II).
- (Previously Presented) The process of claim 22, wherein the propional dehyde is used in a 2.5 to 3.5-fold molar excess based on the aldehyde of formula (II).
- 7 24. (Previously Presented) The process of claim 18 wherein R' is a 4-(2,2,3-trimethylcyclopent-3-en-1-yl) group.
- (Previously Presented) The process of claim 18, wherein the organic solvent in (i) is selected from the group consisting of toluene, xylene, benzene, cyclohexane and methyl cyclohexane.
- 9 26. (Previously Presented) The process of claim 18, wherein R¹ is a saturated alkyl group having from 4 to 16 carbon atoms.
- 10 27. (Previously Presented) The process of claim 18, wherein R¹ is an olefinically unsaturated alkyl group having from 4 to 16 carbon atoms.

28. (Previously Presented) The process of claim 18, wherein R¹ is an olefinically unsaturated cycloalkyl group having from 4 to 16 carbon atoms.

[7 29. (Previously Presented) The process of claim 18, wherein R¹ is not further substituted.

13 36. (Previously Presented) The process of claim 18, wherein R¹ is substituted by an alkyl, cycloalkyl, aryl or alkaryl having up to 12 carbon atoms.

14 31. (Previously Presented) The process of claim 18, wherein R² is hydrogen.

15 32. (Previously Presented) The process of claim 18, wherein R^2 is an alkyl group having from 2 to 6 carbon atoms.

16 23. (Previously Presented) The process of claim 18, wherein said LHSV (liquid hourly space velocity) ranges from 0.6 to 1.2 hr⁻¹.

11 ,34. (Previously Presented) A process for the production of an alkyl-substituted butenol having the formula (I):

$$R^1$$
-CH₂-CH=CR²-CH₂OH (I)

wherein R¹ is a saturated or olefinically unsaturated alkyl or cycloalkyl group having from 4 to 16 carbon atoms and wherein R¹ is optionally substituted by an alkyl, cycloalkyl, aryl or alkaryl having up to 12 carbon atoms; and R² is hydrogen or an alkyl group having from 1 to about 6 carbon atoms the process comprising:

by reacting at least one aldehyde of the formula (II) with at least one corresponding lower aldehyde:

R¹-CH₂-CHO (II)

and R¹ has the same meaning as in formula (I); wherein:

- (i) aldol condensation is carried out in an inert organic solvent, and
- (ii) reduction of the unsaturated aldehydes is carried out in the presence of an optionally calcined copper/zinc catalyst, and

is carried out continuously in a fixed bed reactor at a LHSV (liquid hourly space velocity) of 0.3 to 3.0 hr⁻¹,

under isothermal conditions at a temperature ranging from 45 to 60°C, and under a hydrogen pressure of 1 to 300 bar.